

PUG

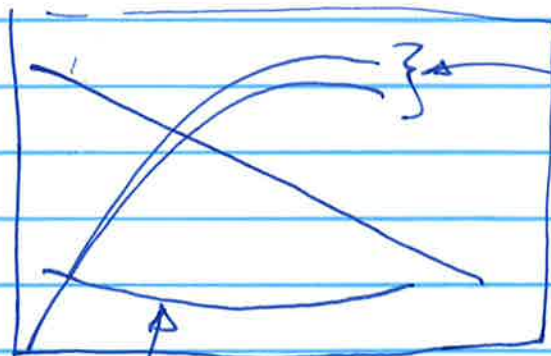
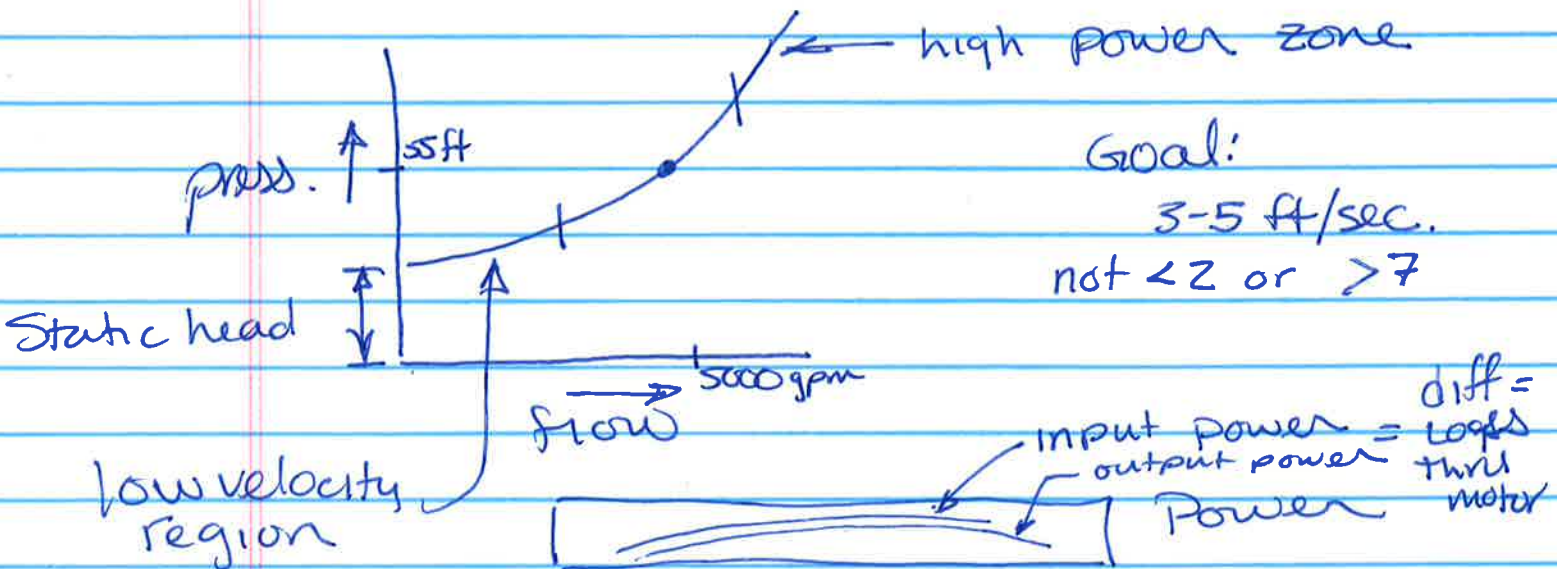
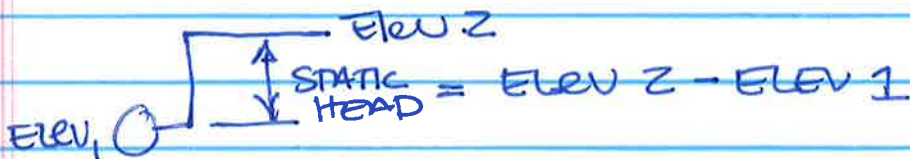
6/11/19

# Duty Point Centrifugal Pumping Basic

Flow Rate (gpm) & Pressure (ft)

500 gpm @ 55 ft

$$TDH = \text{Static} + \text{Dynamic Head}$$

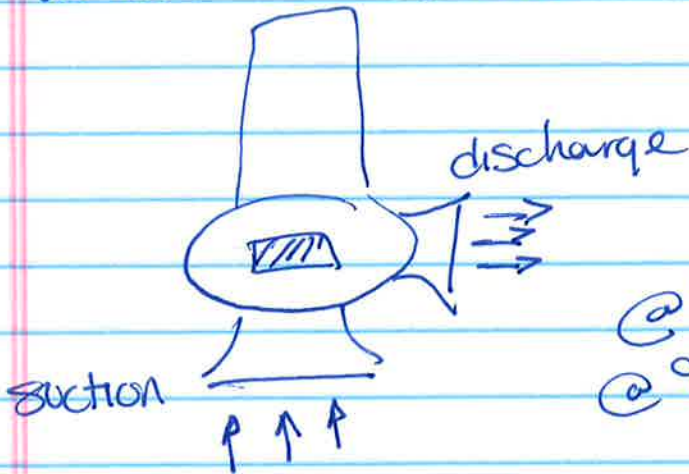


@ discharge flange.

Pump efficiency  
top hydraulic efficiency  
bottom motor efficiency

net positive suction curve

Wire to water efficiency



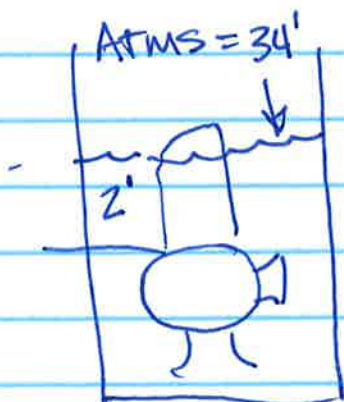
@ 90% efficient pump  
@ 90% efficient motor

Wire to water efficiency  
 $= .90 \times .90 = 81\%$  efficient

Cavitation - where water boils

\* increase velocity  $\Rightarrow$  lowers pressure  
if fluid moves through pump  
fast enough the pressure drops  
to point where no heat req'd for boiling

\* Need min pressure @ impeller  
to keep water from vaporizing

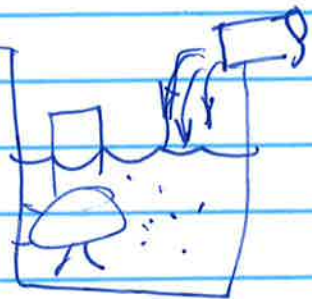


total  $NPSH_a \geq NPSH_R$

$NPSH_a = 34' + z' - \text{suction losses}$

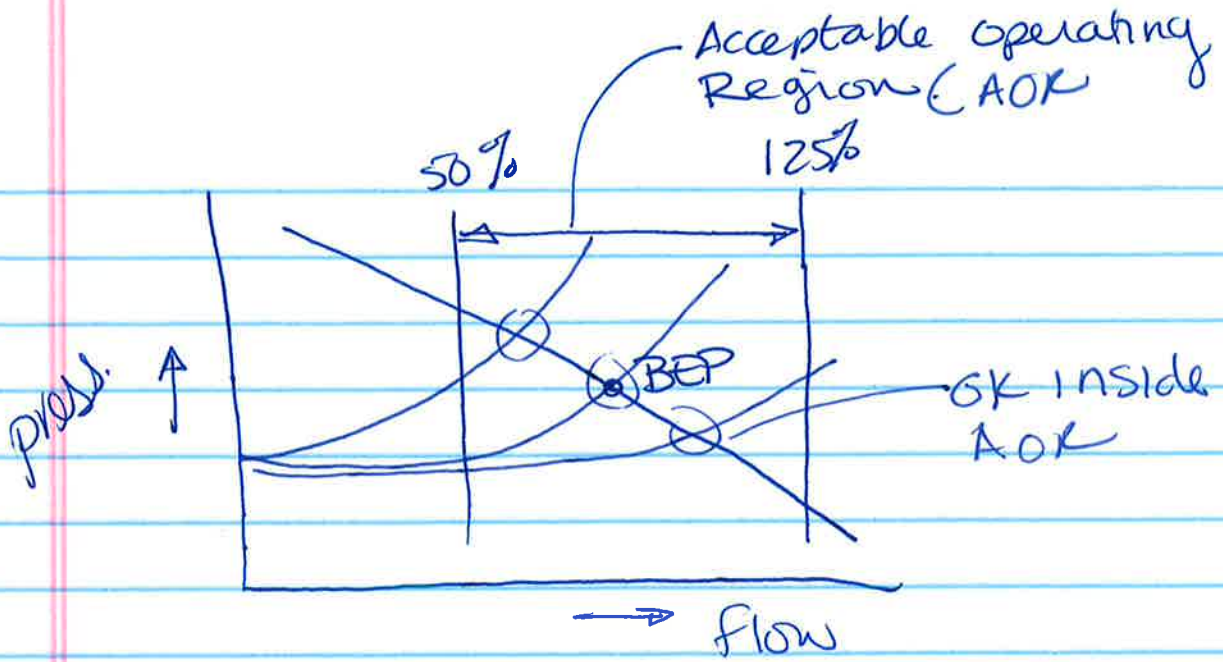
## Cavitation Damage

- \* on Right hand side of curve
  - Insipient cavitation
  - stops pumping - starts again > cyclical
  - damage inside impeller
- \* on left hand side of curve
  - constant sound
  - more vibration
  - even though very low velocity difference in pressures cause recirculation
  - damage on tips of impeller
- \* Air Induced Cavitation
  - entrained air due to turbulence from falling water
  - damage on outside of impeller

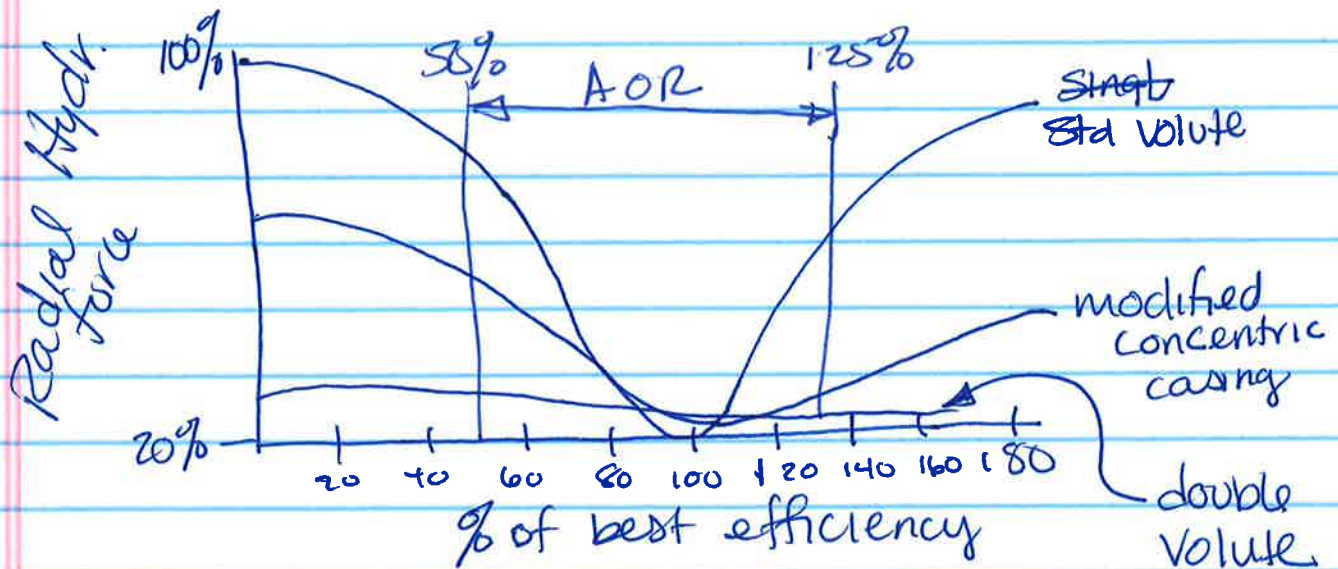


Cavitation can be caused by partially closed valve because velocity increases greatly

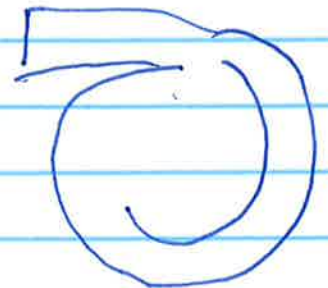
tangential velocity



BEP = Best efficiency point  
 lowest amount of energy per gal pumped

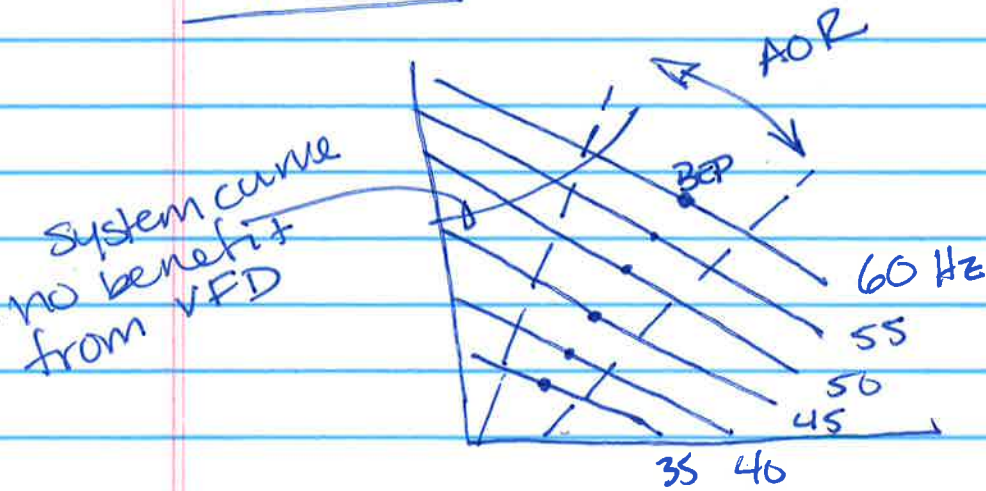


Hydraulic Institute  
 80% → 115%



Check w/ Pump Manufacturer.

# VFDs



BEP is proportional to speed of pump

Adding VFD to existing system

System curve must fit with VFD AOR or turn down will not be possible

radial hydraulic loading goes down with the square of the speed